Sono-emulsion electrosynthesis: electrode-insensitive Kolbe reactions

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The electro-oxidation of water-immiscible liquid aliphatic acids (RCO₂H) leading to decarboxylation to afford a hydrocarbon (R–R) may be achieved using an emulsion formed *via* insonation so that the organic phase continuously extracts the products; in complete contrast to conventional monophasic electrolyses, the type and yield of products obtained from this biphasic Kolbe electrolysis are independent of the electrode material used.

The introduction of power ultrasound into homogeneous solutions has a considerable effect upon mass transport processes due to macroscopic streaming and microscopic interfacial cavitational events; the sonication of biphasic media can result in the formation of an *in situ* emulsion, Primarily due to cavitational events that occur preferentially at the phase boundary. These mechanical forces act to divide droplets again and again forming microdroplets and effectively 'homogenising' the heterogeneous system.

Electrosynthesis in emulsion media is long established.^{5,6} Sono-emulsion systems have considerable potential for application in electrosynthesis because (i) there is no need for emulsion stabilising reagents, (ii) the separation of products is facile, (iii) aqueous solutions may be co-emulsified with a sparingly soluble liquid depolariser, resulting in a medium of high conductivity, (iv) high rates of mass transport can be achieved, and (v) the electrode surface is continually activated.⁷

We report the use of sono-emulsion media to study the electro-oxidation of hexanoic acid (Kolbe reaction). Previous sono-electrosynthetic studies⁸⁻¹² have focussed upon the effects of ultrasound on Kolbe electrolysis, exclusively under monophasic conditions, and with seemingly contradictory data. In this work it is shown that under biphasic conditions, although Kolbe electrolysis is conducted at a potential far beyond that required for solvent decomposition, an efficient conversion of hexanoic acid into decane is achieved at both platinum and boron-doped CVD (chemical vapour deposited) diamond film anodes. Surprisingly, the anode material does not affect the type or ratio of products formed.

An electrochemical cell equipped with an ultrasonic probe§ was used as reported earlier.¹³ With an ultrasound intensity of 190 W cm⁻², this configuration leads to forceful mixing and emulsification of two-phase systems such as water | decane. The biphasic emulsion systems of hexanoic acid (*ca.* 5 mL) in aqueous 1.0 M NaOH (*ca.* 15 ml) had a conductivity of *ca.* 20 mS cm⁻¹ and pH of 6.1. These values were kept more or less constant throughout the electrolysis by the reduction of water at the platinum counter electrode, and the gradual dissolution of the organic acid into the aqueous solution phase.

Power ultrasound was used to emulsify *ca.* 15 mmol of hexanoic acid in an aqueous 1.0 M NaOH biphasic system. After the passage of 1 Faraday (per mole of hexanoic acid) of charge (*ca.* 1500 C, sufficient to quantitatively convert hexanoic acid assuming a one-electron oxidation process) the reaction

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was stopped, excess hydroxide neutralised with acid, and the organic products extracted with ethyl acetate and analysed by GC-MS and NMR spectroscopy. Data summarised in Table 1 describe the conditions used and the yields of the main product, decane—the Kolbe dimer, generated in this electrolysis process. At platinum electrodes, it can be seen that a threshold current density (or applied potential) exists below which the Kolbe process cannot compete against background processes such as oxygen evolution. As in the monophasic case, 14 increasing the temperature at which the reaction takes place causes a decrease in current efficiency; decreasing the aqueous electrolyte concentration also has this effect. The effect of the current density can be rationalised as follows. Initially, increasing the current density causes the current efficiency to improve, and good yields of decane are observed at current densities in the range 0.2–0.3 A cm⁻²; at values of 0.35 A cm⁻² and higher, the current efficiency decreases. This can be rationalised in terms of the flux of hexanoate towards the electrode surface. The ultrasound-determined mass transport limiting current (I_{lim}) in homogeneous solution is given by que eqn. (1):

$$I_{\text{lim}} = \frac{nFADc}{\delta} \tag{1}$$

where n refers to the number of electrons transferred at the electrode, F is the Faraday constant (96485 C mol⁻¹), A is the area of the platinum working electrode (1.1 cm²), D and c refer to the diffusion coefficient and the concentration of hexanoate in the emulsion respectively, and the Nernstian diffusion layer thickness, 1 δ is ca. 5 μ m. Using the Wilke–Chang method¹⁵ for estimation of diffusion coefficients, and further assuming the viscosity of the emulsion to be not too different from that of water, a hypothetical mass transport controlled limiting current

Table 1 Results from galvanostatic electrolysis experiments^a 2 Me(CH₂)₄CO₂H \rightarrow Me(CH₂)₈Me

Mass of hexanoic acid/g	Concentration of NaOH/M	Current density/ A cm ⁻²	Tenperature/K	Yield ^b (%) of decane
1.1 cm ² p	latinum disc anoc	le		
1.72	1.0	0.08	293	0
1.72	1.0	0.13	293	24 ± 3
1.83	1.0	0.18	293	45 ± 5
1.82	1.0	0.35	293	40 ± 5
1.67	0.1	0.18	293	17 ± 2
1.87	1.0	0.18	313	3 ± 1
0.25 cm ²	free-standing poly	ycrystalline bo	oron-doped CVD dia	amond anode
1.80	1.0	0.35	293	40 ± 5
1.80	1.0	0.70	293	14 ± 5

a Reaction conditions: oxidation of hexanoic acid at a 1.1 cm² platinum anode (or at a 0.25 cm² free-standing polycrystalline boron-doped CVD diamond electrode) in an aqueous NaOH/hexanoate emulsion system in the presence of power ultrasound (7 mm electrode-to-horn distance, 190 W cm⁻²). Charge equivalent to 1 Faraday per mol of hexanoic acid was passed before analysis (ca. 1500 C). ^b Yields based upon quantitative analysis of ¹H NMR signals.

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density of up to ca. 1 A cm⁻² may be inferred. Hence, the oxidation is a mass transport controlled process and not limited by electrode kinetics. Increasing the current density beyond the mass transport limit gives rise to additional oxygen evolution rather than the desired Kolbe process, resulting in loss of efficiency. Decreasing the current density below a critical value of ca. 0.1 A cm⁻² causes the Kolbe process to stop as the anode potential falls below the threshold required for Kolbe electrolysis.

The Kolbe dimer is not produced exclusively: GC–MS and NMR analysis of the electrolytic products permits the identification of the ester, amyl caproate, formed in <5% yield. The absence of any pentenes and pentanols is novel and surprising. This is indicative of a trapping of the initial reaction intermediates at the electrode surface; the pentyl carbocation is unlikely to be formed as a free intermediate during electrolysis.

It is widely known that ultrasound damages the surface of platinum electrodes. Pecently, boron-doped CVD diamond electrodes have been employed in the presence of ultrasound with negligible damage to the electrode surface. Furthermore, diamond surfaces are chemically inert under hostile conditions and after long-term electrolysis at very positive potentials. The level of boron doping is high, typically $ca.\ 10^{20}\ cm^3$, corresponding to a B:C atom ratio of 1:1000, allowing a resistivity of 0.3 m Ω m to be achieved.

Galvanostatic electrosynthesis experiments employing a boron-doped CVD diamond anode were conducted at different current densities, and the products analysed as before. The products observed in conventional Kolbe electrolyses suggest that the electrode material exerts a strong control, with products predominantly derived from carbocation intermediates detected at carbon anodes. ¹⁴ Surprisingly, electrosynthesis at a boron-doped CVD diamond anode under sono-emulsion conditions again gives rise to the detection of predominately the Kolbe dimer (see Table 1). Current efficiencies and yields are only slightly lower than those observed at platinum electrodes. Interestingly, the ester, amyl caproate is again the sole byproduct, suggesting that a mechanism similar to that at platinum electrodes is operative.

In summary, Kolbe electrolysis has been accomplished under the novel conditions of an emulsion generated *in situ* by power ultrasound. This method of electrosynthesis renders good yields of product and is highly charge efficient. For the first time in 150 years, ¹⁹ the electrode material used and conditions employed are observed to have only little effect upon the type of products formed. Although the mechanism of the reaction is unclear, it may involve encapsulation of intermediates within the organic component of the emulsion. This type of electrosynthetic methodology shows promise for wider application.

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Notes and references

 \S The ultrasound generator employed was a VCX400 model immersion horn (Sonics and Materials, USA) equipped with a 3 mm diameter stepped titanium-alloy tip (electrically insulated) emitting 20 kHz sound with power level set to 190 W cm $^{-2}$ (calorimetrically determined). The horn-to-electrode distance was maintained at 7 mm. Galvanostatic electrosynthesis was undertaken in the thermostatted cell (volume ca. 20 cm 3) using a PAR 173 (EG&G) galvanostat fitted with a PAR 178 (EG&G) digital coulometer. The cathode employed was a coil of platinum wire; the anode was either a 12 mm diameter platinum disc (Aldrich) or a 5 \times 5 mm free-standing polycrystalline boron-doped CVD diamond plate (DeBeers Industrial Diamond Division, UK). Chemical reagents and NaOH (Aldrich) were of the highest commercially available purity.

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